

Contents lists available at [ScienceDirect](http://www.sciencedirect.com/science/journal/03787753)

Journal of Power Sources

journal homepage: www.elsevier.com/locate/jpowsour

Short communication

Hydrogen storage in carbon fibers activated with supercritical $CO₂$: Models and the importance of porosity

F. Salvador [∗], M.J. Sánchez-Montero, J. Montero, C. Izquierdo

Dpto. Química Física, Plaza de la Merced s/n, Facultad de Ciencias Químicas, Universidad de Salamanca, 37006 Salamanca, Spain

article info

Article history: Received 22 July 2008 Received in revised form 18 November 2008 Accepted 10 January 2009 Available online 20 January 2009

Keywords: $H₂$ storage Activated carbon fibers Supercritical CO₂

ABSTRACT

In this work we studied the adsorption of H_2 at 77 K and 0.0–0.12 MPa onto carbon fibers activated with supercritical CO₂ (ACFs) and with different burn-offs (10-53%). The highest amount of H_2 stored was 2.45 wt% in an ACF with a burn-off of 51% at 0.12 MPa. The measured isotherms were analyzed using an equilibriummodel derived by analogy with amultiple-site Langmuir-type adsorptionmodel. The different equilibria correspond to adsorption in pores of different sizes. The experimental results fitted a model with two different adsorption sites satisfactorily, allowing such sites to be related to the microporous structure of the ACFs. Thus, a high-energy adsorbent–adsorbate interaction site, associated with very small micropores, accessible only to very small molecules such as $H₂$, and another lower-energy site associated with larger pores can be proposed. The model also predicts the adsorption behavior under equilibrium conditions at higher pressures, allowing the maximum adsorption capacity of the ACFs to be determined. The results show that the ACFs adsorb most of the H₂ molecules at low equilibrium pressures, and that they become almost saturated at pressures around 1.0 MPa. The maximum H_2 storage capacity in these ACFs lies between 1.50 and 3.15 wt%.

© 2009 Elsevier B.V. All rights reserved.

1. Introduction

In recent years there has been increasing interest in finding a method for storing H_2 that will allow its use on vehicles. In this sense, the process of adsorption onto carbonaceous materials seems to be one of the most promising [\[1,2\]. R](#page-4-0)esearch in this field is vigorous; some authors have focused on seeking materials and preparation conditions with a view to achieving maximum storage capacity, while others have investigated the relationship between the textural characteristics of the adsorbent materials and their storage capacity. Concerning this latter, there is some controversy in the sense that some investigators have reported a linear dependence of the specific surface area, *S_{BET}*, of the adsorbent on the adsorption capacity [\[3–5\]. O](#page-4-0)thers, in contrast, have proposed that it is the narrowest microporosity that is tightly related to the capacity to adsorb H_2 [\[6–9\].](#page-4-0)

The aim of this work was to focus on a less known aspect; namely the search for an adsorption model that would describe the experimental results in a satisfactory way. The study was carried out with ACFs prepared using a novel procedure of physical activation with supercritical $CO₂$.

2. Experimental

As starting material, a Novoloid phenolic textile fiber supplied by Kynol and carbonized at 750 ◦C in an inert atmosphere of nitrogen was employed. The ACFs were prepared by physical activation of the carbonized fiber using supercritical $CO₂$ (SCCO₂) as the activating agent at 11 MPa and different temperatures: 750, 775 and 800 ◦C. These conditions were kept for several time intervals in order to achieve different burn-off degrees (10–53%). A more detailed description of the experimental details concerning the preparation of the ACFs can be found in previous reports [\[10,11\]. B](#page-4-0)urn-off was determined from the loss of mass undergone by the carbon fibers during the activation process. The nomenclature used to refer to the different series of ACFs is as follows: the activation temperature, followed by "ACF" and finally the percentage of burn-off. Changes in the porosity of the carbonized fibers produced by the different experimental conditions were analyzed from the physical adsorption isotherms of N_2 at 77 K, measured on an automatic volumetric adsorption apparatus, ASAP 2010, from Micromeritics.

The parameters determined were as follows: (i) specific surface area, *SBET*, calculated by applying the BET equation [\[12\]](#page-4-0) to the N_2 adsorption isotherm at 77 K; (ii) micropore volume deduced from application of the Dubinin–Raduskhevich equation [\[13\]](#page-4-0) to the adsorption isotherms, $V_0(N_2)$; (iii) mean pore width, L_{SB} , deduced from the Characteristic Energy by application of the Stoeckli and Ballerini equation [\[14\].](#page-4-0)

[∗] Corresponding author. Tel.: +34 932294478; fax: +34 923294574. *E-mail address:* salvador@usal.es (F. Salvador).

^{0378-7753/\$ –} see front matter © 2009 Elsevier B.V. All rights reserved. doi:[10.1016/j.jpowsour.2009.01.024](dx.doi.org/10.1016/j.jpowsour.2009.01.024)

The $H₂$ storage capacity was determined from the adsorption– desorption isotherms of H_2 at 77 K and at pressures of 0–0.12 MPa, using a Micromeritics Tristar device.

3. Results

3.1. Textural characteristics

The textural characteristics of the carbonized fiber and of the different ACFs are shown in Table 1, together with the corresponding percentage of $H₂$ adsorbed and the average density of hydrogen adsorbed at a pressure of 0.12 MPa and a temperature of 77 K. Calculation of this density was performed based on the amount of H_2 adsorbed and the micropore volume, $V_0(N_2)$, assuming that all the H2 had been homogeneously adsorbed in the micropore. As the starting material, the carbonized fiber already showed very high values of the textural parameters. This indicates the presence of a large incipient microporosity. For the three series of ACFs prepared, S_{BET} and $V_0(N_2)$ increased with the burn-off, reaching maximum values of $1904 \text{ m}^2 \text{ g}^{-1}$ and $0.73 \text{ cm}^3 \text{ g}^{-1}$ for the 775ACF51 sample; i.e., typical of highly microporous materials. This evolution of the porosity with activation may have been favored by the $SCCO₂$ because it penetrates the whole microporous structure of the carbonized fiber more easily, thanks to the pressure applied [\[11\]. T](#page-4-0)hus, a highly uniform activation must have occurred, with a widening of the micropores, since the start of activation. The ACFs selected in this work covered a broad range of micropore sizes: from 0.49 nm to 1.19 nm.

In Table 1 it may also be seen that the ACFs rapidly increased the amount of H_2 adsorbed when the burn-off was increased and at the same time the density of the H_2 adsorbed decreased.

Fig. 1 shows the evolution of the amount of H₂ adsorbed *versus* $V_0(N_2)$. All the ACFs, regardless of the experimental conditions used in their preparation, increased the amount of H_2 adsorbed as $V_0(N_2)$ increased. A similar kind of behavior was found upon correlating the amount of H_2 adsorbed with the S_{BET} . Different authors have reported linear relationships between the adsorption capacity and some of these textural parameters [\[7\]. H](#page-4-0)owever, as seen in Fig. 1 for these fibers the correlation is not linear, pointing to a less marked increase in the H_2 adsorbed for the highest $V_0(N_2)$ values.

Fig. 2 shows the density of hydrogen adsorbed at a pressure of 0.12 MPa against mean micropore width. It may be seen that density increased rapidly with the decrease in mean micropore width. Sample 775ACF11, with a pore width of 0.51 nm, is the one showing the highest density: 0.053 g cm−3. This density is close to that of liquid H₂ at 1 atm and 20.3 K (0.0708 g cm⁻³), pointing to the strong interaction between the surface of the ACF and the H_2 . Theoreti-cal studies [\[15–17\]](#page-4-0) have shown that the maximum packing of H_2

Fig. 1. Evolution of the H₂ stored with micropore volume.

Fig. 2. Variation in the density of H₂ adsorbed with micropore width.

molecules is achieved in pores whose width ranges between 0.36 and 0.56 nm. This very high storage density, 0.053 g cm⁻³, which is achieved by having the H_2 adsorbed in the pores at an equilibrium pressure of 0.12 MPa, would be equivalent to having the H_2 stored in

a deposit at a pressure of 22.8 MPa. Of all the fibers prepared, sample 775ACF51 was the one that adsorbed the most H_2 (2.45 wt%). However, it was not the sample with the greatest H_2 packing but the one with the greatest $V_0(N_2)$ and S_{BET} . This value for the H₂ adsorption capacity is in agreement with those reported by other authors [\[18,6,19\]. C](#page-4-0)urrently, amounts of adsorbed H_2 greater than 5 wt% can be reached at 77 K, but at high pressures. The greatest adsorption capacities tend to correspond to chemically activated and super-activated carbons [\[20\].](#page-4-0)

Moreover, if the volume occupied by the fiber (0.8 g cm^{-3}) is taken into account, simple calculations show that the H_2 stored per unit volume at the equilibrium pressure of 0.12 MPa in the 775ACF51 sample would be equivalent to having the H_2 stored without adsorbent at a pressure of 6.1 MPa.

All these findings highlight the advantage of using an adsorbent to store hydrogen and suggest that there is a close relationship between the microporosity of the fibers and their capacity to adsorb $H₂$.

3.2. Adsorption isotherms

We obtained the adsorption–desorption isotherms of $H₂$ at 77 K from 0.0 to 0.12 MPa for all the ACFs prepared and the carbonized fiber. Fig. 3 shows the isotherms plotted on the linear and logarithmic scales of the 775ACF series. The adsorption isotherms are in agreement with the desorption isotherms and no hysteresis was observed, pointing to the reversibility of the adsorption and that it is physical.

All the isotherms have similar shapes: Type I according to the IUPAC classification. The carbonized fiber adsorbed a large amount of H_2 . For pressures lower than 3 kPa, the amount of H_2 adsorbed decreased slightly with the increase in burn-off. However, for pressures higher than this the trend was reversed, and the amount of H_2 adsorbed increased with burn-off in a more marked fashion. This kind of behavior occurs because the smaller micropores of the carbonized fiber decrease progressively with burn-off while the larger micropores increase in number [\[11\].](#page-4-0)

This shape of the isotherms has been confirmed by different authors for the adsorption of H_2 on different carbonaceous materials, suggesting that they can be satisfactorily fitted to the Langmuir equation [\[5,21\].](#page-4-0) [Fig. 4](#page-3-0) shows the fitting to that equation for the isotherms corresponding to two fibers with different burn-offs. In all cases, this Langmuir model cannot fit the experimental data well, showing that the $ACF/H₂$ adsorption system is complex.

3.3. Two-site adsorption model

A much more precise correlation was obtained when the experimental results were fitted to a Langmuir model with two energetically different adsorption sites:

$$
n = \frac{n_1 K_1 p}{1 + K_1 p} + \frac{n_2 K_2 p}{1 + K_2 p}
$$

where *n* is the amount of H_2 adsorbed at equilibrium per unit mass of adsorbent at the equilibrium pressure p ; n_i is the maximum amount of H₂ adsorbed at site *i*, which is achieved when the adsorption site is filled, and K_i is the affinity constant or Langmuir constant, which provides information about the strength with which the molecule of adsorbate is bound to site *i*. All the isotherms are very precisely correlated with this model. [Fig. 4](#page-3-0) shows this correlation together with the contribution of each site for two ACFs with different burn-offs. In all cases, site 1 was rapidly saturated, even at low equilibrium pressures and low burn-offs. Site 2, except for very low pressures, adsorbed more H_2 than site 1 and was only saturated at greater pressures.

[Table 2](#page-3-0) shows the values of the parameters n_i and K_i for the carbonized fiber and all the ACFs prepared. Site 1 is saturated and retains almost the same amount of H_2 for any burn-off, although the strength of adsorption is very high and progressively declines with burn-off. Also, the maximum amount of H_2 that can be retained by site 2 is greater than that of site 1 and increases with burn-off. Nevertheless, the strength of $H₂$ adsorption at this site is much smaller than that seen for site 1 and also decreases as burn-off increases. This behavior of sites 1 and 2 suggests that site 1 may be associated with very small micropores and site 2 with larger ones. The high values of K_1 and the low values of K_2 clearly indicate that sites 1 and 2 are very different and may be identified with very small micropores, where the adsorbent–adsorbate interactions are very strong, and larger micropores, where such interactions are small respectively.

From the four parameters it is possible to predict the adsorption capacity for different equilibrium pressures. The sum of n_1 and n_2 provides the maximum adsorption capacity of the fiber [\(Table 2\).](#page-3-0) [Table 2](#page-3-0) also shows the amounts of H_2 adsorbed by all the ACFs extrapolated to the equilibrium pressure of 1.0 MPa, and it may be seen that for that pressure the ACFs are very close to saturation. These findings show that at low pressures (>0.12 MPa) the adsorption capacity of the ACFs increases rapidly with temperature. However, at higher pressures the increase is much less

Fig. 3. H₂ adsorption isotherms at 77 K: (a) linear form; (b) logarithmic form.

Fig. 4. Fitting of two isotherms to the Langmuir equation and to the Langmuir double equation with the contribution of each of the sites.

Table	
-------	--

Parameters of the Langmuir double equation and maximum amount of H₂ storage.

pronounced, such that at 1.0–1.5 MPa the fibers are almost completely saturated. Thus, for example, the 775AC51 fiber adsorbed 2.45 wt% at 0.12 MPa and 3.03 wt% at 1.0 MPa, its maximum adsorption capacity being 3.15 wt%. Fig. 5 shows the evolution of K_2 with the mean pore width for the three series of activated fibers and the carbonized fiber. Again, it may be seen that the value of K_2 is independent of the temperature at which the samples were prepared and that it decreases sharply with pore width. This decrease

Fig. 5. Variation in the K_2 parameter with micropore width.

Fig. 6. Dependence of the maximum amount of H₂ retained at site 2 on micropore volume.

is similar to the variation in the density of the $H₂$ adsorbed with the pore size shown in [Fig. 2. T](#page-1-0)his behavior was expected because when the pores are very narrow the adsorbent–adsorbate interactions are very strong and the packing density is very high. However, when the pores are widened, the packing density declines sharply, as do the adsorbent–adsorbate interactions [15].

Additionally, the amount of H_2 adsorbed in site 2, n_2 , shows an almost linear increase with the micropore volume, $V_0(N_2)$, [Fig. 6.](#page-3-0) Nevertheless, the amount of H_2 retained in site 1, n_1 , remains almost constant for all burn-offs, such that it is not directly related to the evolution of the different textural parameters.

All the above findings suggest that the carbonized fiber contains very small micropores that are hardly widened at all during the activation process since the activating agent $(CO₂)$ is unable to penetrate them. Furthermore, neither they are detected by the N_2 used in the textural characterization, although they are accessible to H2 thanks to the small size of this molecule. These micropores would thus be identified with site 1 and the other larger ones with site 2.

4. Conclusions

Three series of ACFs prepared at 750, 775 and 800 ◦C have been used to study $H₂$ adsorption at 77 K in the 0.0–0.12 MPa pressure range. In all three series the amounts of $H₂$ adsorbed increased steadily with the burn-off and $V_0(N_2)$ volume, and was independent of the activation temperature.

The maximum amount of H_2 stored at 0.12 MPa was 2.45 wt% for the 775AC51 fiber. This fiber has the highest S_{BET} and $V_0(N_2)$, and yet it shows the lowest parking density of H₂ molecules (0.034 g cm⁻³). This density is quite high taking into account the density of liquid H₂ (0.0708 g cm⁻³).

The Langmuir adsorption model with two sites satisfactorily reproduces the behavior of the adsorption of H_2 in these ACFs. The site with the greatest energy adsorbed only a small amount of $H₂$, although with great strength, and became saturated at very low pressures; around 0.12 MPa. This site would be associated with very small micropores, not accessible to $N₂$ molecules. In contrast, the lower-energy site would retain much more H_2 , although only weakly, becoming saturated at higher pressures. The model also provided information about the maximum amount of H_2 that can be stored in the ACFs and allows the amount of adsorbed H_2 to be extrapolated to higher pressures. For all the ACFs assayed, H_2 was mainly adsorbed in the pressure range tested (0.0–0.12 MPa), the materials becoming saturated at pressures around 1.0 MPa.

Acknowledgments

Financial support from the Ministerio de Educación y Ciencia, Spain and European Regional Development Fund (Project CTQ2006- 00759/PPQ) and Junta de Castilla y León (Project SA054A07) is acknowledged.

References

- [1] A.C. Dillon, M.J. Heben, Applied Physics A: Materials Science and Processing 72 (2001) 133–142.
- [2] F. Lamari Darkrim, P. Malbrunot, G.P. Tartaglia, International Journal of Hydrogen Energy 27 (2002) 193–202.
- [3] M.G. Nijkamp, J.E.M.J. Raaymakers, A.J. van Dillen, K.P. de Jong, Applied Physics A 72 (2001) 619–623.
- [4] R. Ströbel, L. Jörissen, T. Schliermann, V. Trapp, W. Schütz, K. Bohmhammel, G. Wolf, J. Garche, Journal of Power Sources 84 (1999) 221–224.
- B. Panella, M. Hirscher, S. Roth, Carbon 43 (2005) 2209-2214.
- [6] K. Mark Thomas, Catalysis Today 120 (2007) 389–398.
- [7] L.L. Vasiliev, L.E. Kanonchik, A.G. Kulakov, D.A. Mishkinis, A.M. Safonova, N.K.
- Luneva, International Journal of Hydrogen Energy 32 (18) (2007) 5015–5025. [8] N. Texier-Mandoki, J. Dentzer, T. Piquero, S. Saadallah, P. David, C. Vix-Guterl, Carbon 42 (2004) 2735–2777.
- [9] W.-C. Xu, K. Takahashi, Y. Matsuo, Y. Hattori, M. Kumagai, S. Ishiyama, K. Kaneko, S. Iijima, International Journal of Hydrogen Energy 32 (13) (2007) 2504–2512.
- [10] F. Salvador, M.J. Sánchez Montero, C. Izquierdo, Journal of Physical Chemistry C 111 (2007) 14011–14020.
- [11] M.J. Sánchez Montero, F. Salvador, C. Izquierdo, Journal of Physical Chemistry C 112 (37) (2008) 4991–4999.
- [12] F. Salvador, C. Sánchez-Jiménez, M.J. Sánchez-Montero, A. Salvador, Studies in Surface Science and Catalysis 144 (2002) 379–386.
- [13] M.M. Dubinin, Chemistry Reviews 60 (2) (1960) 235–241.
- [14] F. Stoeckli, L. Ballerini, Fuel 70 (1991) 557.
- [15] M. Rzepka, P. Lamp, M.A. de la Casa-Lillo, Journal of Physical Chemistry B 102 (1998) 10894.
- Q. Wang, J.K. Johnson, Journal of Chemical Physics 110 (1999) 577.
- [17] M.A. de la Casa-Lillo, F. Lamari-Darkrim, D. Cazorla-Amorós, A. Linares-Solano, Journal of Physical Chemistry B 106 (2002) 10930–10934.
- [18] M. Jordá-Beneyto, F. Suarez-García, D. Lozano-Castelló, D. Cazorla-Amorós, A. Linares-Solano, Carbon 45 (2007) 293–303.
- [19] M.Z. Figueroa-Torres, A. Robau-Sánchez, L. de la Torre-Sáenz, A. Aguilar-Elguézabal, Microporous and Mesoporous Materials 98 (2007) 89–93.
- [20] W.-C. Xu, K. Takahashi, Y. Matsuo, Y. Hattori, M. Kumagai, S. Ishiyama, K. Kaneko, S. Iijima, International Journal of Hydrogen Energy 37 (2007) 2504–2512.
- [21] X.B. Zhao, B. Xiao, A.J. Fletcher, K.M. Thomas, Journal of Physical Chemistry B 109 (2005) 8880–8888.